



Carbon dioxide Capture & Storage (CCS)

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IEA Greenhouse Gas R&D Programme

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Overview of Presentation

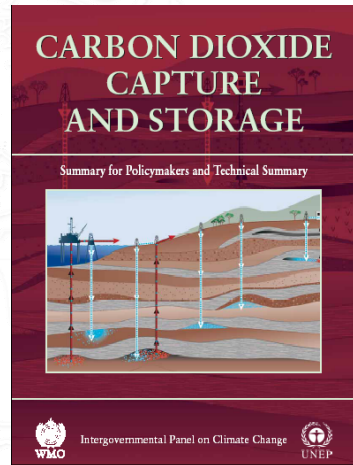
- Introduction
- CCS Projects
- CCS Options and Economics
- Is NH_3 an 'early CCS opportunity' ?
- Summary & Conclusions

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CCS now an option

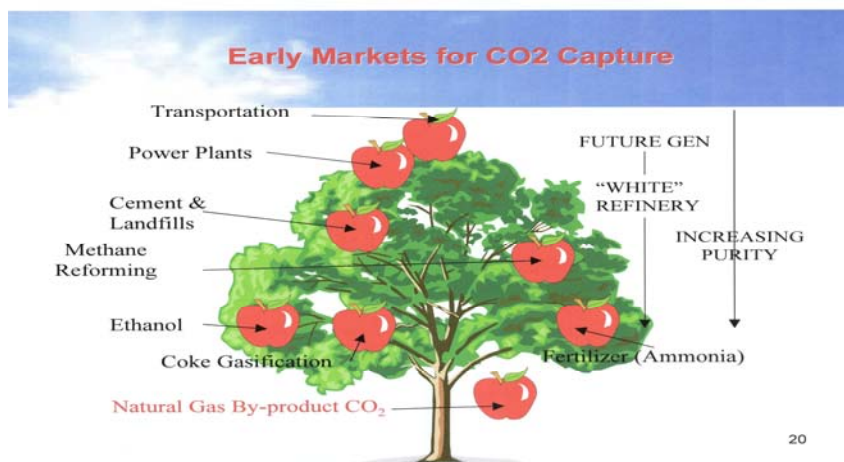
- Significant progress in this area
- IPCC Special Report on CO₂ capture and storage
 - CCS recognised as a mitigation option
 - National emissions accounting
 - Emissions trading



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NH₃ quoted as an 'Early-Opportunity'



Original believed to be from CSLF

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CCS Projects & Technology Status

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Commercial-scale CCS operations

Sleipner

Snøhvit

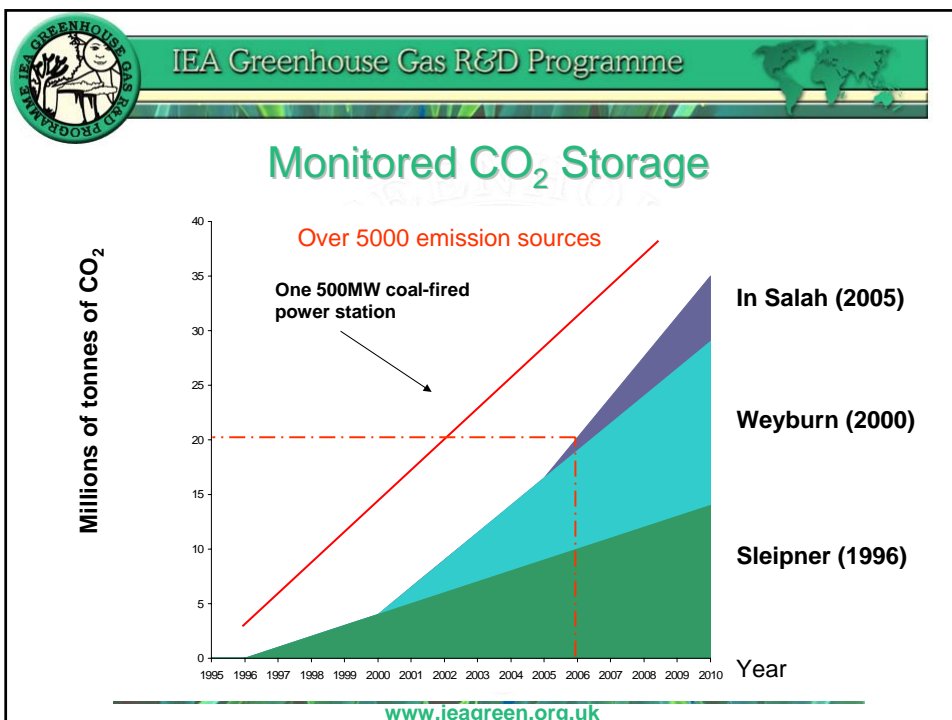
Weyburn

In-Salah

NOT POWER GENERATION

Images Courtesy of BP, Statoil, and PTRC

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- ### Existing activities
- Most actual activity is in the oil and gas sector
 - CO₂ Capture
 - Amine scrubbing demonstrated at 1Mt/y scale in oil and gas field operations
 - Sleipner and In-Salah
 - Not power generation
 - 3100km pipelines mostly in North America transporting CO₂ for EOR operations
 - Several large projects injecting CO₂ at 1Mt/y scale
 - Sleipner and In-Salah – deep saline aquifers
 - Weyburn – oil field
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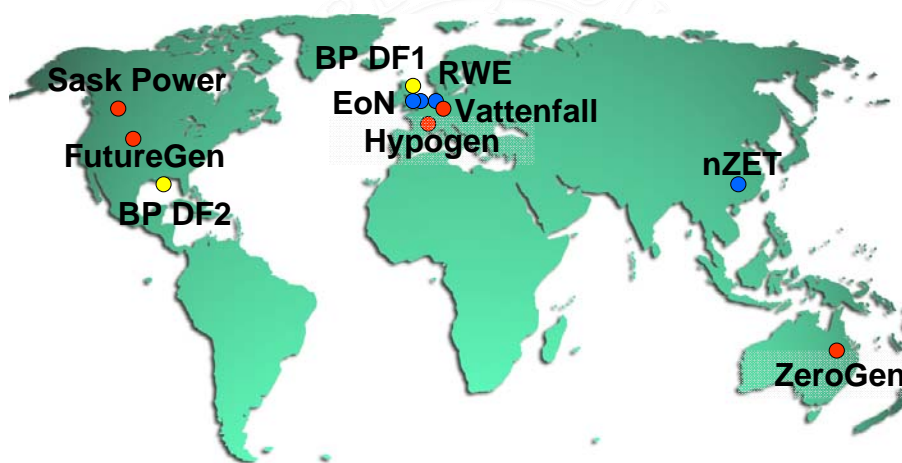


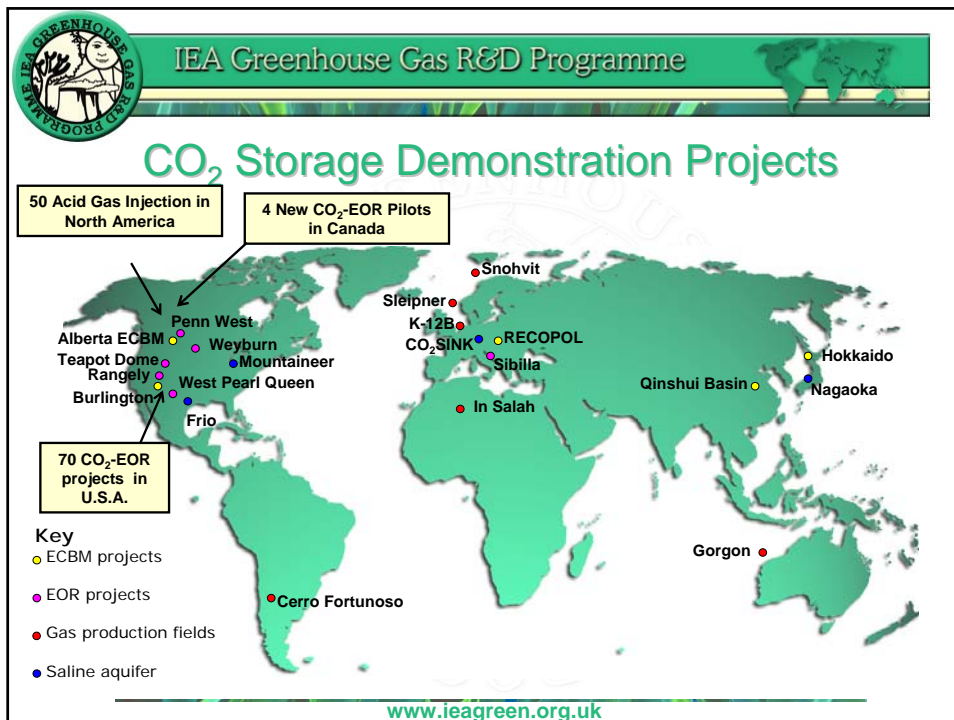
International Acceptance

- Kyoto Protocol route:
 - The Clean Development Mechanism (CDM)
 - CDM option was raised at COP11/MOP1 but a decision was deferred – for 2 years!
 - Outstanding issues from COP/MOP:
 - Permanence
 - Additionally
 - Project boundaries
 - Project leakage
- Storage under the sea bed
 - Important breakthrough in 2006 – sets precedent
 - Storage under seabed will be legal under terms of London Convention 1996 Protocol



Power Sector CCS Projects





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Near-term Implementation

- Currently we are seeing developments in the gas sector
 - CO₂ removal required to meet gas pipeline standards
 - Low incremental cost for CCS
- CO₂-EOR projects not developing as could have been expected worldwide
 - High oil prices could be expected to stimulate development of EOR projects

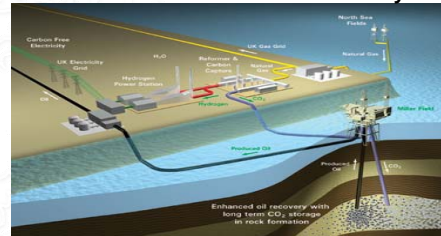
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CO₂-EOR opportunities

Courtesy BP

- North Sea seen as an opportunity for CO₂-EOR
- Studies by NPD and UK DTI said that it is uneconomic
 - CO₂ supply and infrastructure requirements
- New commercial projects now being planned
 - BP DF1 development at the Miller field
 - Statoil/Shell 'Halten' development



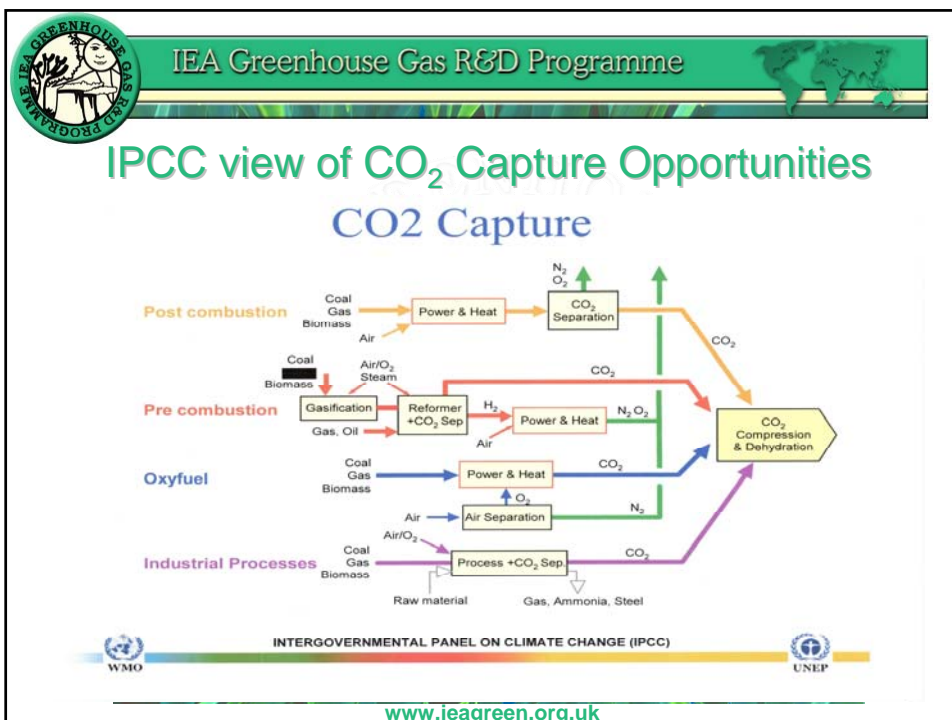
Courtesy Shell/Statoil

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CCS Options & Economics

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IPCC view of CCS costs

CCS component costs

CCS component	Cost range
Capture from a power plant	15 - 75 US\$/tCO ₂ net captured
Capture from gas processing or ammonia production	5 - 55 US\$/tCO ₂ net captured
Capture from other industrial sources	25 - 115 US\$/tCO ₂ net captured
Transportation	1 - 8 US\$/tCO ₂ transported per 250km
Geological storage	0.5 - 8 US\$/tCO ₂ injected
Ocean storage	5 - 30 US\$/tCO ₂ injected
Mineral carbonation	50 - 100 US\$/tCO ₂ net mineralized

20-30% cost reduction over next 10 yrs

Monitoring/verification: 0.1-0.3 US\$/t CO₂

INTERGOVERNMENTAL PANEL ON CLIMATE CHANGE (IPCC)

WMO UNEP

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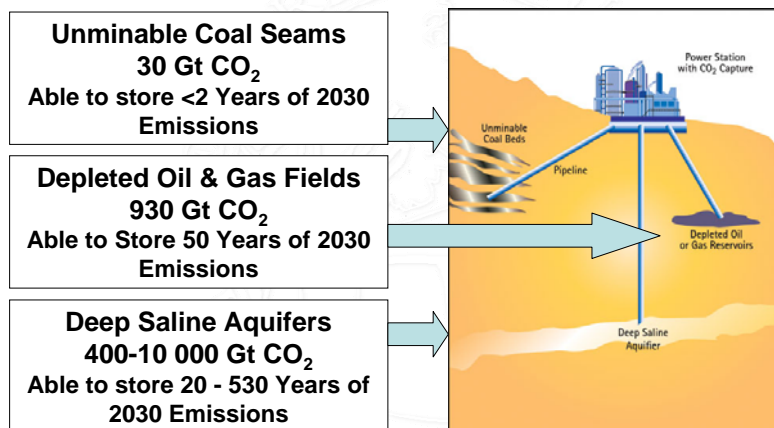
COST OF CO₂ SUPPLY

	US\$/tonne CO ₂
Capture	25-35
Transmission	5-10
Storage	5-10

Overall Cost of CO₂ from CCS is about 35 - 55 US\$/tonne CO₂. Cost of 'early opportunity' CO₂ could be about 10-20 US\$/tonne



Geological storage: Options



Note: CO₂ Storage capacity at cost of 20 US \$ per tonne of CO₂



Is Ammonia Production an Early Opportunity ?

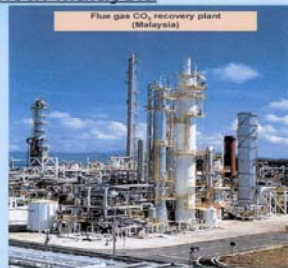


CO₂ Capture an integral part of NH₃ production

MITSUBISHI CO₂ Recovery Technology from Flue Gas

Commercial Scale Plants

1. CO₂ Recovery Plant in Malaysia



Flue gas CO₂ recovery plant (Malaysia)

Plant Outline

CO ₂ recovery capacity	200 ton/day
Solvent	KS-1
Use of CO ₂	Urea production
Start of operation	October, 1999
Client	Petronas Fertilizer (Kedah) Sdn Bhd
Location	Kedah Darul Aman, Malaysia
Flue gas source	Stream reformer flue gas

Process Description

CO₂ is recovered from flue gas of steam reformer of ammonia plant and delivered to CO₂ compressor for urea synthesis. Recovered CO₂ is used to increase urea production. The first commercial plant for flue gas CO₂ recovery using this advance technology has been operating in Malaysia since October 1999 for Urea production. Performance of process is excellent in terms of low steam consumption, very low solvent degradation and low solvent loss.



IPCC emission factors

- $\text{tCO}_2/\text{tNH}_3$
 - 1.7 for modern plant - natural gas feedstock
 - 1.2 process & 0.5 heat & power
 - 2.8 for modern partial oxidation
 - 2.1 average for existing plant – natural gas
 - 3.3 average for existing plant – partial oxidation
- $\text{tCO}_2/\text{t urea}$
 - 0.73

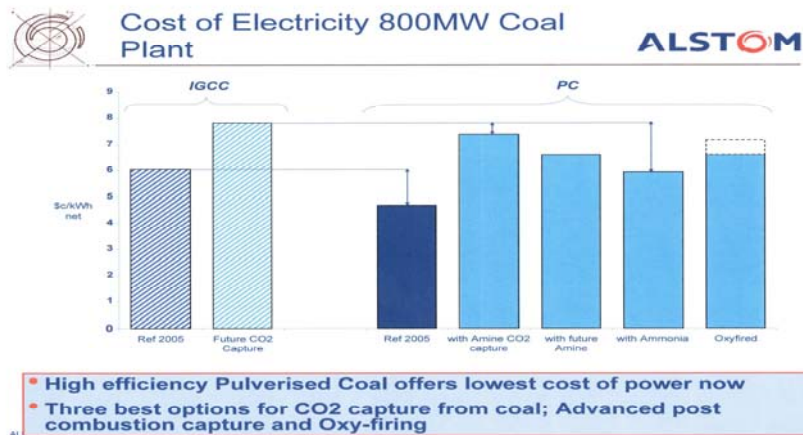


CO₂ balance on ammonia/urea complex

- Global figures (year 2000)
 - 155 million tonnes CO₂ surplus to urea requirements
- Modern complex (private communication)
 - 2000mtpd NH₃ and 3200mtpd urea
 - Excess CO₂ 1064mtpd
 - Most of excess is flue gas not process gas



Ammonia is potentially a capture solvent



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Summary and Conclusions

- CCS is now a firm policy option for CO₂ emission reduction
- Commercial-scale activities are in progress and CCS is gaining credibility
- The financial incentives are not in place
- Early opportunities could help establish CCS
- Further work would be useful to examine ways & means by which NH₃ production could be established as an early opportunity

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Current Membership























* Formalities pending

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