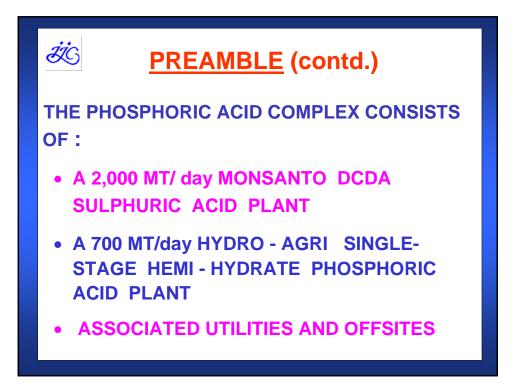
#### USE OF SUB COMMERCIAL(60-65 TCP) ROCK PHOSPHATE IN HEMI PHOSPHORIC ACID PLANT-CHALLENGES AND OPPORTUNITIES

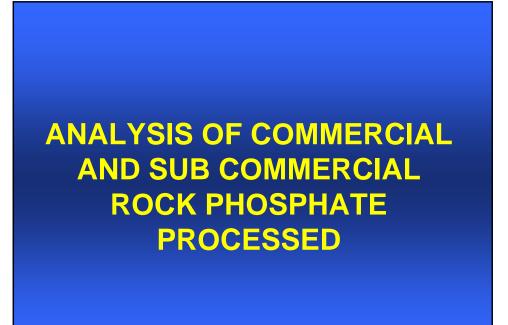


CONTENT
•PREAMBLE
•ANALYSIS OF COMMERCIAL AND SUB COMMERCIAL
ROCK PHOSPHATE PROCESSED
•EVALUATION OF PLANT PERFORMANCE
•QUALITY OF PHOSPHORIC ACID PRODUCED
•MAIN PROBLEMS FACED AND SOLUTIONS ADOPTED
•OPTIMUM BLEND RATIO OF SUB COMMERCIAL ROCK PHOSPHATE
•BENEFITS FROM USE OF SUB COMMERCIAL ROCK
PHOSPHATE
•FUTURE PROSPECTS FOR SUB COMMERCIAL ROCK
PHOSPHATE
•CONCLUSION









	ANALYSIS OF COMMERCIALROCK PHOSPHATE PROCESSED												
Description	Description 1998 1999 2000 2001 2002 2003 2004 2005												
ТСР	70.52	70.57	71.07	71.13	71.78	71.93	72.25	71.73					
P <sub>2</sub> 0 <sub>5</sub>	32.28	32.30	32.52	32.55	32.85	32.92	33.07	32.83					
CaO	48.82	48.00	48.15	49.14	50.25	50.44	50.72	50.18					
CO2	4.13	3.47	3.60	3.83	3.99	4.19	4.22	3.56					
SiO <sub>2</sub>	4.63	6.37	6.41	4.68	4.09	4.39	3.05	4.24					
Fluoride	3.08	2.97	3.38	3.70	3.91	3.76	3.77	2.94					
Chloride	0.025	0.04	0.039	0.049	0.068	0.040	0.04	0.04					
Al <sub>2</sub> O <sub>3</sub>	0.31	0.26	0.22	0.29	0.35	0.36	0.40	0.47					
Fe <sub>2</sub> O <sub>3</sub>	0.19	0.32	0.25	0.25	0.31	0.25	0.27	0.35					
Moisture	15.90	15.25	14.59	14.68	14.82	14.99	15.83	13.30					

# COMMERCIAL ROCK PHOSPHATE PROCESSED

Description	1999	2000	2001	2002	2003	2004	2005
ТСР	63.06	63.59	64.77	63.68	62.32	62.74	61.81
P <sub>2</sub> 0 <sub>5</sub>	28.86	29.10	29.64	29.14	28.52	28.71	28.29
CaO	41.44	42.80	44.64	44.72	43.73	44.13	43.36
CO2	3.02	3.55	3.56	3.93	4.02	3.72	3.60
SiO <sub>2</sub>	14.59	14.92	9.98	10.62	11.36	10.43	10.41
Fluoride	2.52	3.11	3.52	3.61	3.65	3.70	2.87
Chloride	0.036	0.0	0.047	0.081	0.081	0.08	0.082
Al <sub>2</sub> O <sub>3</sub>	0.27	0.27	0.37	0.61	0.64	0.76	0.77
Fe <sub>2</sub> O <sub>3</sub>	0.49	0.45	0.41	0.52	0.50	0.55	0.59
Moisture	15.56	15.01	11.05	5.93	4.28	5.21	3.68

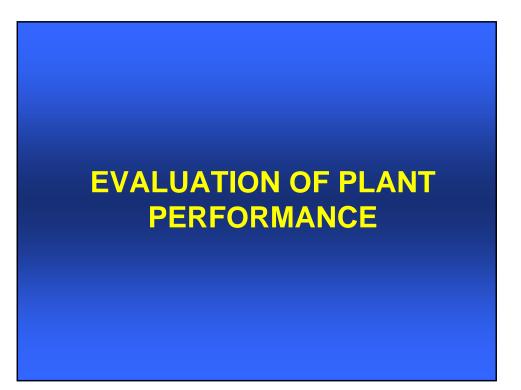
COMPARISON OF COMMERCIAL & SUB COMMERCIAL ROCKS										
Commercial (70 -Sub commercialDescription72 TCP) rockrock (60-65 TCP)%minmaxaveminmaxave										
CaO/P2O5	1.480	1.534		1.436	1.537	1.507	0%			
F/SiO2 R2O3/P2O5	0.466 0.014	1.236 0.025	0.774 0.018			0.289 0.036	63% -94%			
R2O/P2O5	0.013	0.018	0.015	0.015	0.020	0.017	-9%			
F/P2O5 CO2/P2O5	0.090 0.108	0.119 0.128	0.105 0.119	0.087 0.105		0.114 0.126	-8% -6%			

## COMPARISON OF COMMERCIAL & SUB COMMERCIAL ROCKS

- 1. The silica content is much higher in sub commercial rock due to low TCP content.
- 2. The CaO/P2O5 ratio is almost same in commercial and sub commercial rocks, even though there is wide difference in TCP content.
- 3. The R2O3/P2O5 ratio in sub commercial rock is more than that of commercial rock.
- 4. The other constituents are high on relative basis.

## COMPARISON OF COMMERCIAL & <u>SUB COMMERCIAL ROCKS</u>

- 5. In other words, for one MT of P2O5 production, the total amount of constituents (R2O3, R2O, F, SiO2 etc) fed to the reactors is much higher when sub commercial rock is processed compared to that of commercial rock.
- 6. Accordingly, suitable changes in process parameters and operating procedures / equipment, based on the blending ratio, have been employed.



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### FEED ROCK QUALITY

Year	Yearly wt.	Yearly wt.
Tear	Av.TCP (%)	Av.P2O5 (%)
1998	70.55	32.29
1999	70.36	32.20
2000	69.00	31.58
2001	67.76	31.01
2002	66.18	30.29
2003	64.83	29.67
2004	64.46	29.50
2005	63.76	29.18

<b>PLANT PERFORMANCE</b>										
Veer	Production	On stream	Capacity	Onstream	Onstream					
Year	(MT P2O5)	days achieved	Utilisation (%)	Factor (%)	efficiency (%)					
1998	237,874	325	106	89	119					
1999	224,847	314	100	86	117					
2000	224,123	288	100	79	127					
2001	192,010	257	86	70	122					
2002	250,422	325	112	89	126					
2003	231,884	326	104	89	116					
2004	218,523	330	98	90	108					
2005	229,307	324	102	89	115					



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- The yearly average TCP content in rock fed to the reactors got reduced from 70.55 (1998) to 63.76 (2005), as the ratio of sub commercial rock fed is increased.
- During the year 2002, the average TCP content was 66.18, and highest capacity utilization of 112% was achieved.

#### **PLANT PERFORMANCE**

- The on stream days achieved during the years 2002 to 2005 (around 50% is sub commercial rock) are around 325 days and almost same as that achieved during the year 1998 (100% commercial rock) as against the design stream days of 320.
- The on stream efficiency is maintained well above 100% during the period 1998 to 2005 even while using sub commercial grade rock phosphate by optimization of critical process parameters.

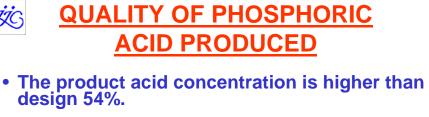


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- The specific consumption of raw materials and chemicals has increased when high blend ratios of sub commercial rock are used.
- The plant maintenance expenditure has also increased during last three years.

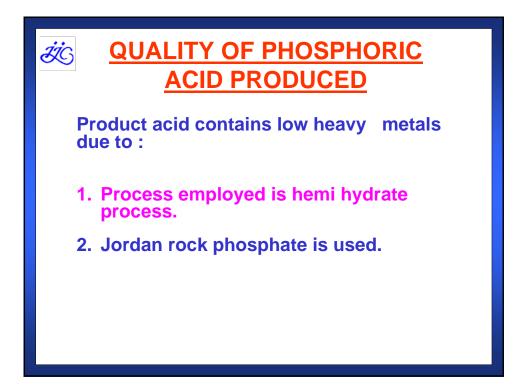
### QUALITY OF PHOSPHORIC ACID PRODUCED

Image: Constraint of the second sec									
	Year P2O5 (%) R2O3 / P2O5								
	1998 54.51 0.008								
	1999 54.14 0.015								
	2000	56.17	0.020						
	2001	56.30	0.019						
	2002	56.39	0.022						
	2003 55.95 0.024								
	2004	56.12	0.024						
	2005	55.95	0.029						

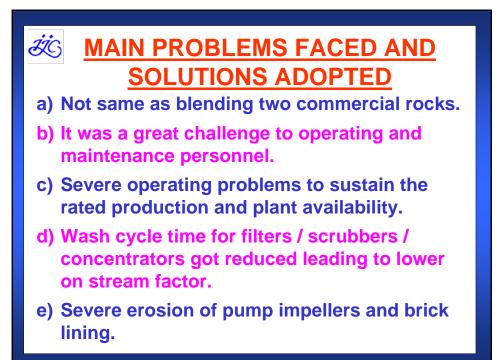


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- Product acid concentration is maintained at 56% since 2000 to reduce transportation costs, even though sub commercial rock was used.
- Lower throughput from concentrators due to high R2O3 and low P2O5 in feed acid.
- Increase of R2O3 in product acid, but within the acceptable range.







## MAIN PROBLEMS FACED AND<br/>SOLUTIONS ADOPTED

A. Foreign materials in rock phosphate

- Foreign materials (hard stones, metals pieces etc) were noticed in rock supplies.
   Damages to the rock feeder belts, conveying equipment and cause severe erosion in reactors.
- Two vibrating screens were introduced, Additionally, grids are provided for all underground rock feeders (extractors for the storage piles).

#### **MAIN PROBLEMS FACED AND** SOLUTIONS ADOPTED

#### B. Coarse material in rock phosphate

- Larger than 2 mm (design 100% < 2 mm) is noticed. Settling in first reactor without undergoing any reaction. Severe erosion of carbon brick lining of the reactors.
- Increasing the quality checks. Periodically draining the first reactor and recycling the decanted acid. Additional layer of brick lining at critical areas of reactors.

# Image: Main Problems faced and<br/>Solutions adopted

#### C.Reaction system

- For a given rock feed rate, the P2O5 fed to reactors is lower and impurities are higher as the blending ratio increases. Wide fluctuation in reaction parameters.
- Modification of plant water balance and optimisation of process parameters. Slurry parameters in last reactor (R2) are: P2O5 – 38 to 40%, Solid content – 29 to 32% w/w and SO4 – 1.6 to 2.0%. No change in reaction temperatures.

## MAIN PROBLEMS FACED AND SOLUTIONS ADOPTED

#### D. Filtration system

- Filter cake produced is higher as the blending ratio is increased.
- Wash ratios and filter cycle time are slightly reduced to optimise the filtration efficiency and the acid concentration. The speed of the vacuum pumps is increased to meet the additional vacuum load and higher plant loads. The width of the filter cloth is increased by 100 mm.

## MAIN PROBLEMS FACED AND SOLUTIONS ADOPTED

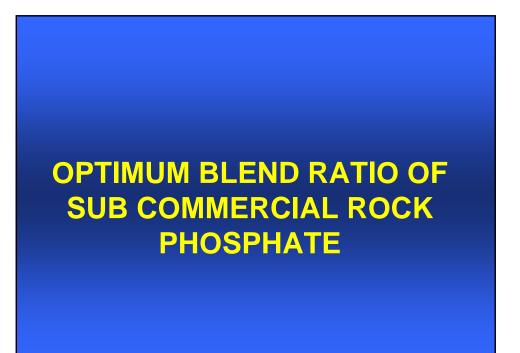
E. Gas Scrubbing system

- Total silica content is high. 70 to 80% of total silica is reactive. Frequent fouling of gas scrubbing system.
- The concentration / temperature of circulating liquor in scrubbing system are reduced. The frequency of manual cleaning increased to once in a month. One additional scrubbing fan is installed.

## MAIN PROBLEMS FACED AND SOLUTIONS ADOPTED

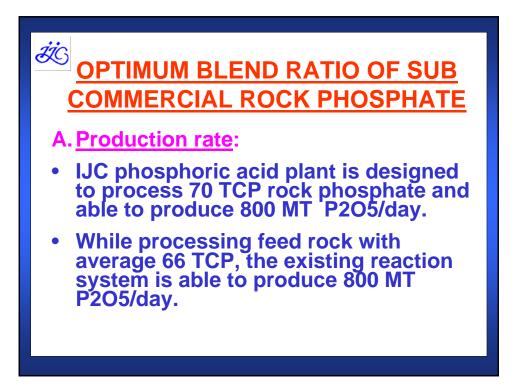
#### F. Concentration system

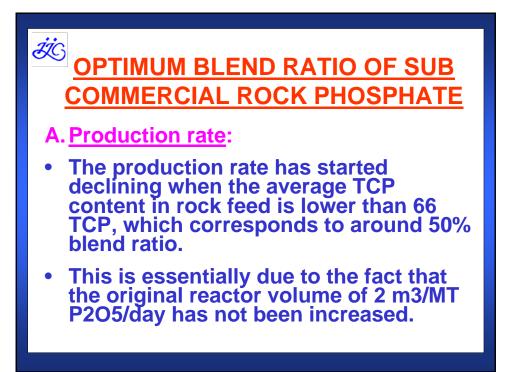
- Filter acid concentration is lower at 38-40%. The throughput from the existing two concentrators is not adequate.
- Additional recycling of sludge settled in product storage tank (56% P2O5) to filter acid storage tank (40% P2O5) to increase the acid concentration to 42% P2O5. Addition of a third concentration unit of same capacity during May 2005.

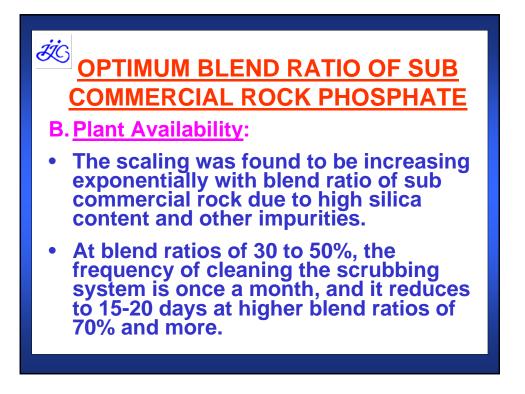


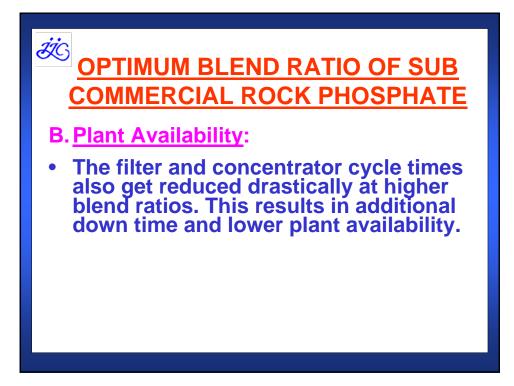
# OPTIMUM BLEND RATIO OF SUB COMMERCIAL ROCK PHOSPHATE Production rate

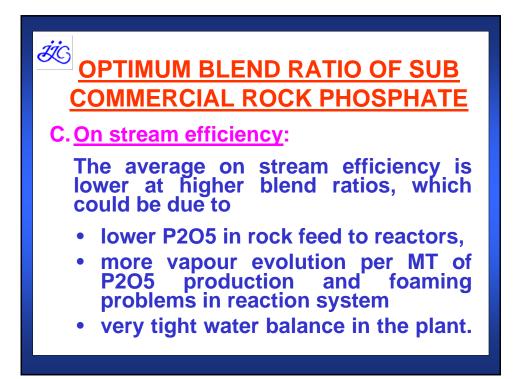
- Plant Availability
- On stream efficiency
- Maintenance / Chemicals cost

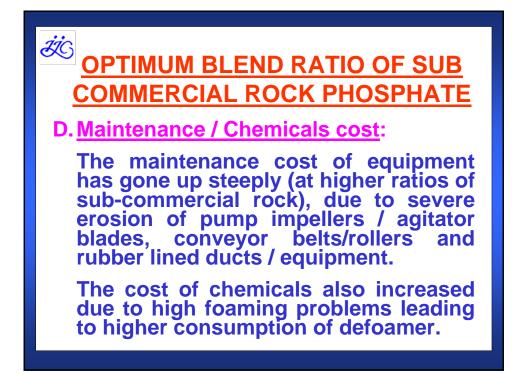








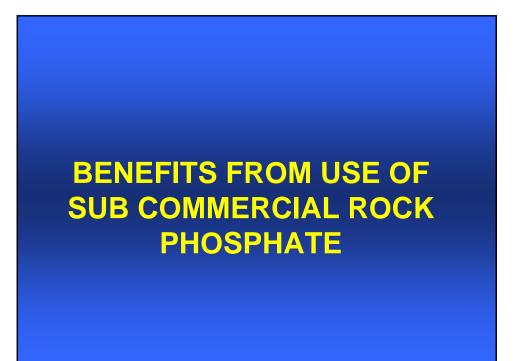






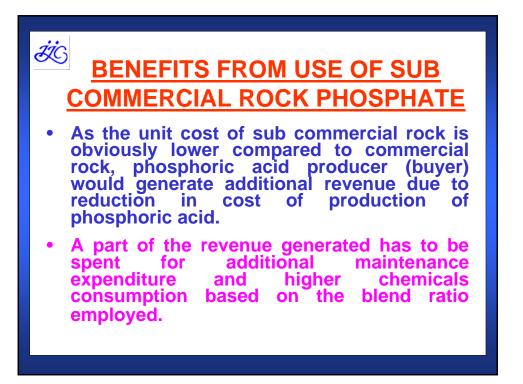
### OPTIMUM BLEND RATIO OF SUB COMMERCIAL ROCK PHOSPHATE

Considering the overall plant performance (production rate, plant availability, on stream factor and maintenance/chemicals cost) as well as the various technical problems higher blend faced at ratios, the recommended optimum blend ratio is 50% to derive maximum benefits from the use of sub commercial rock phosphate.



### BENEFITS FROM USE OF SUB COMMERCIAL ROCK PHOSPHATE

- It is unique situation wherein both the buyer and the seller of rock phosphate would benefit.
- As the sub commercial rock needs to be disposed off suitably, phosphate producer (seller) needs to incur an additional expenditure. If this rock phosphate were supplied to/used in phosphoric acid plant, this would generate an additional revenue for the seller due to value addition to the sub commercial rock phosphate.







### FUTURE PROSPECTS FOR SUB COMMERCIAL ROCK PHOSPHATE



## FUTURE PROSPECTS FOR SUB COMMERCIAL ROCK PHOSPHATE Scenario 2:

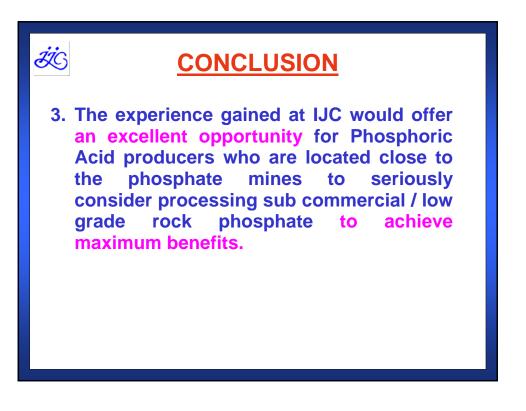
For those plants, which are located / being located close to the phosphate mines, use of sub commercial rocks, as a blend, would eventually be an economical proposition, though suitable technical solutions/practices need to be considered.



#### **CONCLUSION**

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- 1. Use of sub commercial or low grade rock phosphate at optimum blend ratio with commercial rock phosphate is technically feasible and the overall plant performance can be maintained at almost the same level as that achieved with the use of commercial rock alone.
- 2. The optimum blend ratio for continuous plant operation is 50% for deriving the maximum benefits from plant availability as well as on stream efficiency keeping the maintenance / Chemicals costs at reasonable level.





### **PLANT PERFORMANCE**

washings         (#)         washing           1998         71         74         145         42         42         -         84           1999         46         47         93         41         45         -         86           2000         43         38         81         27         38         -         65           2001         22         29         51         22         22         -         44           2002         31         33         64         40         37         -         77           2003         39         32         71         30         36         -         66           2004         30         29         59         45         43         -         88           2005         30         33         63         26         25         14         65	Year	Filte	r washing	details	Co	Concentrator washing details			
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		Filter - I	Filter - II		Conc - I	Conc - II			
1999       46       47       93       41       45       -       86         2000       43       38       81       27       38       -       65         2001       22       29       51       22       22       -       44         2002       31       33       64       40       37       -       77         2003       39       32       71       30       36       -       66         2004       30       29       59       45       43       -       88         2005       30       33       63       26       25       14       65				wasnings			(#)	wasnings	
2000         43         38         81         27         38         -         65           2001         22         29         51         22         22         -         44           2002         31         33         64         40         37         -         77           2003         39         32         71         30         36         -         66           2004         30         29         59         45         43         -         88           2005         30         33         63         26         25         14         65	1998	71	74	145	42	42	-	84	
2001         22         29         51         22         22         -         44           2002         31         33         64         40         37         -         77           2003         39         32         71         30         36         -         66           2004         30         29         59         45         43         -         88           2005         30         33         63         26         25         14         65	1999	46	47	93	41	45	-	86	
2002         31         33         64         40         37         -         77           2003         39         32         71         30         36         -         66           2004         30         29         59         45         43         -         88           2005         30         33         63         26         25         14         65	2000	43	38	81	27	38	-	65	
2003         39         32         71         30         36         -         66           2004         30         29         59         45         43         -         88           2005         30         33         63         26         25         14         65	2001	22	29	51	22	22	-	44	
2004         30         29         59         45         43         -         88           2005         30         33         63         26         25         14         65	2002	31	33	64	40	37	-	77	
2005 30 33 63 26 25 14 65	2003	39	32	71	30	36	-	66	
	2004	30	29	59	45	43	-	88	
	2005	30	33	63	26	25	14	65	
# Concentrator III was commissioned during May 2005.		# Concer	ntrator III w	as commissi	oned durii	ng May 200	)5.		